

AN ENHANCED NUMERICAL ONE-DIMENSIONAL TRANSIENT  
FUEL ROD CODE FOR LIGHT WATER REACTORS

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نموذج عددي محسني احادي الابعاد لدرجات الحرارة الغير مستقره  
في قضبان الوقود النووي لمفاعلات الماء الحميم

تهدف هذه الورقة الى بحث التطور الزمني لدرجات الحرارة في قضبان الوقود النووي لمفاعلات الماء الحميم وذلك في الحالة الغير مستقره ، وذلك بتطوير نموذج رياضي عددي احادي الابعاد ، ويعتمد هذا النموذج على تحويل المعادله التفاضليه لتوصيل الحرارة الغير مستقره مع وجود مصدر طاقة داخلي الى معادله جبريه ، ويقسيم قضيب الوقود في الاتجاه القطري الى رقائق اسطوانيه وتطبيق المعادله الحصريه على كل رقيقه نحصل على مجموعه من المعادلات الاتيه التي يمكن حلها مع اعتبار الشروط الحدوديه . وتتميز هذه الطريقة بطول الفتره الزمنيه الازمه لشرط للحصول على حل عددي مستقر وذلك باستخدام الطريقه الصريحه والتي تتميز ببساطتها وسرعة الحل . كما تم في هذا العمل تعديل معادله تحليليه رياضيه للتوصيل الحراري الغير مستقر في قضيب وقود غير مغلف وذلك لتطبيقها على قضيب مغلف . وتدل النتائج على ان الحل العددي المقترح يعطي نتائج تتفق مع الحل التحليلي المعقد والذي يحتاج ايضا الى برمجيه . كما تدل النتائج على ان درجه حرارة سطح الغلاف تحل الى الحالة المستقره اسرع من درجه حرارة مرشح الوقود عند أي معدل لانتاج الطاقه الداخليه .

ABSTRACT

In this paper a new enhanced simple numerical fuel rod code is developed, which is used to calculate the transient one-dimensional fuel temperature behavior in Light Water Reactors. The proposed code is then applied to determine the transient temperature behavior of fuel due to sudden rise in heat generation rate. The obtained results are then compared with that obtained from an analytical transient solution. The steady state values obtained from both solutions are then compared with that obtained from the corresponding closed form solution of this problem. It is proved that the numerical code is more powerful and accurate.

INTRODUCTION

Heat conduction with internal heat generation is an important problem in the fields of nuclear and electrical engineering. Solid reactor and radioisotopic fuel rods and electrical resistance heaters are elements in which heat is both generated and conducted. Temperature development in both steady and transient operation is important in evaluating reactor core thermal performance. The amount of power generation in a given reactor is limited by thermal rather than by nuclear considerations [1,2]. The reactor core must be operated such that with adequate heat removal system, the temperature of the fuel and cladding anywhere in the core must not exceed safe limits. The behavior of the

fuel-coolant combination in response to reactivity insertions, loss of coolant, or other transient effects is of vital importance. In case of loss of coolant accident, the time after which the fuel or cladding meltdown temperatures is reached is very important, therefore a *fuel rod code* is used in conjunction with a nuclear code, core code, and loop code to determine the temperature behavior of cladding surface [3].

Exact analytical solutions of this problem in only a few cases for different geometries may exist. Exact solution to the transient, one-dimensional form of the heat equation have been developed for an infinite bare cylinder with internal heat generation [2,4]. The solution with surface condition which is characterized by convective heat transfer coefficient  $h_{eff}$  is as follows [2]:

$$T^* = \sum_{n=1}^{\infty} (C_n / \zeta_n^2) \cdot (1.0 - \text{EXP}(-\zeta_n^2 \text{Fo})) \cdot J_0(\zeta_n r^*) \quad (1)$$

$$\begin{aligned} \text{where } T^* &= (T - T_a) / T_o, & T_o &= (q''' R_o^2) / k \\ C_n &= (2 / \zeta_n) [J_1(\zeta_n) / (J_0^2(\zeta_n) + J_1^2(\zeta_n))] \\ r^* &= r / R_o, & \text{Fo} &= k\theta / (R_o^2 \rho C), & \text{Bi} &= h_{eff} R_o / k \end{aligned}$$

and the discrete values (eigenvalues)  $\zeta_n$  are positive roots of the transcendental equation

$$\zeta_n \frac{J_1(\zeta_n)}{J_0(\zeta_n)} = \text{Bi}$$

The quantities  $J_1$  and  $J_0$  are Bessel functions of the first kind.

According to [2] it can be shown that for values of  $\text{Fo} \geq 0.2$ , the infinite series solution can be approximated by the first term of the series.

In light water reactors, the coolant in the core is considered as a boundary condition which supplies the fuel rods with a sink temperature and a heat transfer coefficient. Conduction in the radial direction is usually taken into account [5,6] and some codes consider conduction in the axial conduction also. With nonuniform cooling, conduction in the azimuthal direction must be considered [7]. Thermal radiation from rod-to-rod is negligible when the core is filled with liquid. There are many fuel rod codes to predict the steady and transient temperature behavior of nuclear fuel rods. The problem is to improve the time and space of computation. For this purpose, the present fuel rod code is developed, in which one dimensional transient heat conduction is taken into account.

#### MATHEMATICAL PROCEDURE

The general heat conduction equation is given by

$$\nabla^2 T + \frac{q'''}{k} = \frac{\rho C}{k} \frac{\partial T}{\partial \theta} \quad (2)$$

To transform the above equation into algebraic equation, the time variable  $\theta$  and space variable  $r$  are broken into discrete intervals  $\Delta\theta$  and  $\Delta r$  as shown in Fig.(1).

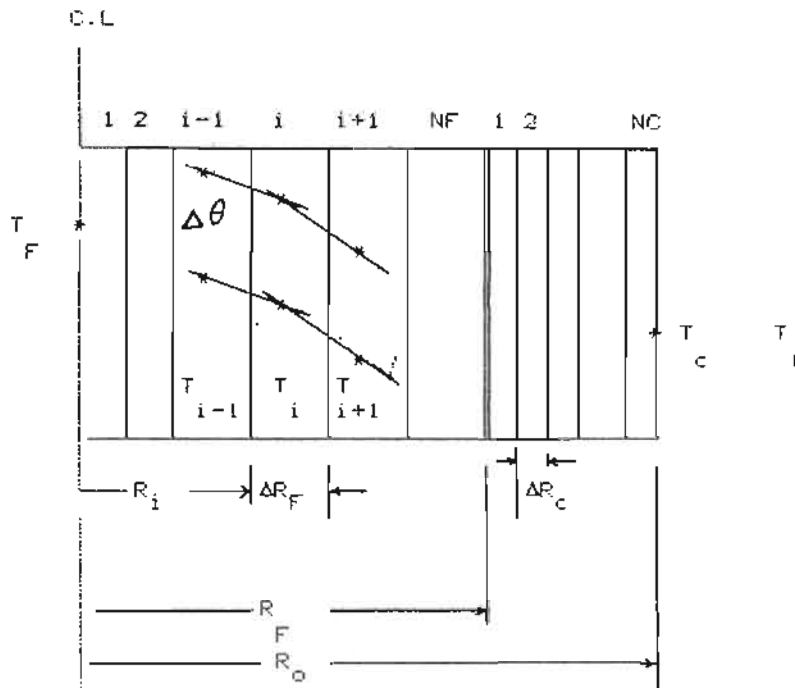


Fig. 1 Nodes in one-dimensional cylindrical system

Applying Eq.(2) to the nodal point  $i$  for one dimensional Laplacian in cylindrical coordinates and rearranging, one get the following linear equation :

$$T_i^{\theta+\Delta\theta} = (1-F_1-F_2)T_i^\theta + F_1T_{i-1}^\theta + F_2T_{i+1}^\theta + FO \Delta T_g \quad (3)$$

where

$$F_1 = \frac{2FO P_i \Delta R}{A}, \quad F_2 = \frac{2FO R_{i+1} \Delta R}{A}$$

$$A = R_{i+1}^2 - R_i^2, \quad FO = \frac{k \Delta\theta}{\rho c \Delta R^2}$$

and

$$\Delta T_g = \frac{q'' \Delta R^2}{k}$$

The following boundary conditions are applicable for the considered case :

\* For the innermost layer  $i = 1$ , we have

$$\left(\frac{\partial T}{\partial r}\right)_{r=0} = 0.0$$

To satisfy this condition , the coefficient  $F_1$  must equal zero.

\* For the outermost cladding layer  $i = N$ , we have

$$\left(\frac{\partial T}{\partial r}\right)_{r=R_o} = - (\alpha/k_c) \cdot (T_N - T_F)$$

To satisfy the above condition, the coefficients  $F_1, F_2$  are given

by:

$$F_1 = \frac{2(FD)_c R_N \Delta R_c}{(R_o^2 - R_N^2)}, \text{ and}$$

$$F_2 = \frac{2(FD)_c h R_o \Delta R_c^2}{k_c (R_o^2 - R_N^2)} = \frac{2(FD)_c (Bi)_c \Delta R_c^2}{(R_o^2 - R_N^2)} \quad (4)$$

To account for the effect of the helium gas gap at the interface between the fuel surface and the inner cladding surface, the coefficients  $F_1$  and  $F_2$  for both the last fuel layer NF and the first cladding layer NF+1 are given by :

\* For the layer  $i=NF$

$$F_1 = \frac{2(FD)_F R_{NF} \Delta R_F}{(R_{NF+1}^2 - R_{NF}^2)}$$

$$F_2 = \frac{2(FD)_F R_{NF+1} \Delta R_F^2}{k_F (R_{NF+1}^2 - R_{NF}^2) [(\Delta R_F/2k_F) + (1/h_g) + (\Delta R_c/2k_c)]} \quad (5)$$

\* For the layer  $i=NF+1$

$$F_1 = \frac{2(FD)_c R_{NF+1} \Delta R_c^2}{k_c (R_{NF+2}^2 - R_{NF+1}^2) [(\Delta R_F/2k_F) + (1/h_g) + (\Delta R_c/2k_c)]}$$

$$F_2 = \frac{2(FD)_c R_{NF+2} \Delta R_c}{(R_{NF+2}^2 - R_{NF+1}^2)}$$

Each body of the fuel and cladding is divided into a number of concentric cylindrical layers of equal thickness  $\Delta R_F$  and  $\Delta R_c$ , Fig.(1). Applying Eq.(3) to each layer one gets a system of finite difference equations. There are several methods for the solution of a system of simultaneous linear equations [2,4,5,6,8]. The forward difference technique (explicit scheme) is however simpler but is not unconditionally stable, while the backward technique (implicit scheme) is unconditionally stable but more complex [4,6,8]. The forward differences applied in the present code result in errors that are proportional to  $\Delta r^2 \Delta \theta$  [2,8]. A KWU 1300 MWe pressurized water reactor is chosen as an illustration example [9]. The following data are required :

Average volumetric heat generation rate  $q_{av}''' = 3. \times 10^9 \text{ W/m}^3$

Inlet temperature  $291^\circ \text{C}$ ,

Fuel rod pitch = 12.7 mm,

Fuel is  $\text{UO}_2$ ,

Cladding is Zircaloy-4,

Pellet radius  $R_F = 4.025 \text{ mm}$ ,

Cladding thickness = 0.64 mm,

Fuel rod outside radius  $R_o = 4.75 \text{ mm}$ ,

Fuel rod active height  $H = 3.9 \text{ m}$ ,

$h = 4.0 \times 10^4 \text{ W/m}^2 \text{ deg}$  [5-7],  $h_g = 4500 \text{ W/m}^2 \text{ deg}$  [5-7]

$$k_F = 2.50 \text{ W/m.deg.}, \rho_F = 10200 \text{ Kg/m}^3, c_F = 296 \text{ J/Kg.deg.}$$

$$k_c = 15.13 \text{ W/m.deg.}, \rho_c = 630 \text{ Kg/m}^3, c_c = 319 \text{ J/Kg.deg.}$$

For simplicity, material properties are considered temperature independent and the heat transfer coefficient  $h$  is assumed constant along the length of the fuel rod. First, the maximum fuel temperature and its corresponding coolant and cladding temperatures are calculated analytically using separate subroutine. The developed code is then applied at this section. The volumetric heat generation rate  $q'''$  obeys the relation:

$$q''' = q_c''' \cos(\pi z/H_e) = (\pi/2) q_{av}''' \cos(\pi z/H_e)$$

where  $q'''$  and  $q_c'''$  are the volumetric heat generation rate at any point  $z$  and the center of the fuel element, and  $H_e$  is the extrapolated fuel element height ( $H_e \approx H$ ).

#### RESULTS AND DISCUSSION

To examine the validity of the proposed code, the time behavior of temperature in a clad fuel rod is estimated using the proposed code and the results are compared with that obtained from the infinite series solution given by Eq.(1), which is also computerized using the approximate series of Bessel functions [10].

To make sure that the solution converges, the coefficients of the finite difference equation (Eq. (3)) must be positive. Applying this principle to the outer most cladding layer where the term  $F$  is the largest term because it includes the heat transfer coefficient  $h$ .

$$(1 - F_1 - F_2) \geq 0.0$$

Substituting for  $F_1$  and  $F_2$  from Eqs.(4), one obtains,

$$(FO)_c \leq \frac{1}{2 \left[ \frac{R_N \Delta R_c}{R_o^2 - R_N^2} + \frac{(Bi)_c \Delta R_c^2}{R_o^2 - R_N^2} \right]} \quad (6)$$

and the time step  $\Delta\theta$  is then given by:

$$\Delta\theta = (\rho C)_c \Delta R_c^2 (FO)_c / k_c \quad (7)$$

The above stability criteria can be approximately reduced to:

$$\Delta\theta \leq \frac{(\rho C)_c \Delta R_c^2}{k_c + \Delta R_c h} \quad (8)$$

which about twice the time interval used in [5].

It is concluded that the new condition improves the economics of computations due the higher time interval  $\Delta\theta$ .

The analytical calculations (Eq.(1)) are conducted considering the effective heat transfer coefficient given by:

$$h_{eff} = \frac{1}{\frac{1}{h_g} + \frac{R_F}{k_c} \ln(R_I/R_F) + \frac{R_F}{P_o h}} \quad (9)$$

The effective heat transfer coefficient of the considered case

takes the convection through the gas gap, the conduction through the cladding material, and the convection through the coolant into consideration. Using the corresponding values  $h_{eff}$  is then calculated and has the value of  $3481 \text{ W/m}^2\cdot\text{K}$ .

Using the proposed code for fluid temperature of  $311^\circ\text{C}$  one gets the numerical solution as shown in figure (2). Fig.(2) illustrates the time behavior of fuel temperature for a normal cooling channel ( $q'''=3.0 \times 10^8 \text{ W/m}^3$ ). According to the figure it is clear the fuel centerline temperature reaches the steady value  $970^\circ\text{C}$  in approximately 27 second. Comparing this value of the centerline temperature with the analytically obtained corresponding value ( $948^\circ\text{C}$ ) a well agreement is found. In addition, the numerically obtained values lie above the analytical values, which means more conservative solution is obtained. Another important fact is that the steady state values obtained numerically is closer to that obtained from the closed form analytical steady state closed form solution which is given by:

$$T_F - T_f = \frac{q'''R_F^2}{4k_F} + \frac{q'''R_F^2}{2} \left[ \frac{1}{k_c} \ln \frac{R_o}{R_F} + \frac{1}{h R_o} \right] + \frac{q'''R_F}{2h_g} \quad (10)$$

According to the relation (10), the steady state fuel centerline temperature for the considered case is  $974^\circ\text{C}$ , while the analytical transient solution (Eq.(1)) gives the value of  $948$  and the value obtained numerically is  $970^\circ\text{C}$ .

Figures (3) and (4) illustrate the temperature behavior for different volumetric heat generation rates  $q'''$ . It is clear that raising the neutron flux from zero to the value which produces  $6.0 \times 10^8 \text{ W/m}^3$  in a hot channel leads to raising the fuel temperature from initial value of  $311^\circ\text{C}$  to a steady value of  $1629^\circ\text{C}$  in approximately 30 seconds, while the cladding temperature reaches the value of  $337^\circ\text{C}$ . This steady state fuel temperature is less than the melting point of the UO<sub>2</sub> fuel material which is  $2749^\circ\text{C}$  [2]. In addition, the obtained values of fuel and cladding temperature are comparable to the values obtained from the closed form solution given by Eq. (10) ( $1636$  and  $337^\circ\text{C}$ ), while the value obtained from the analytical transient solution (Eq.(1)) is  $1584^\circ\text{C}$ . Investigating the time behavior of fuel and cladding temperatures as shown on Figs.(2) and (4), it can be deduced that the surface of the cladding reaches its stable temperature faster than the fuel centerline temperature. This is because the thermal diffusivity of the cladding material ( $7.5 \times 10^{-6} \text{ m}^2/\text{s}$ ) is higher than that of the fuel material ( $8.3 \times 10^{-7} \text{ m}^2/\text{s}$ ).

#### CONCLUSIONS

From the above discussion it is concluded that the proposed code is structurally simple and requires small storage capacity. Consequently, the speed and accuracy of the calculations are greatly enhanced. In addition, even though exact analytical solutions may be available a numerical technique might prove economical and convenient.

## NOMENCLATURE

Bi	Biot Number = $h R_o / k_c$
C	Specific heat (J/Kg.deg.)
F	Coefficients (dimensionless)
Fo	Fouriers modulus = $k \Delta\theta / (\rho c \Delta R^2)$
h	Cladding to fluid heat transfer coefficient (W/m <sup>2</sup> deg)
h <sub>g</sub>	Gas heat transfer coefficient (W/m <sup>2</sup> deg)
h <sub>eff</sub>	Effective heat transfer coefficient (Eq.(9))
H	Fuel element active height (m)
k <sub>∞</sub>	Thermal conductivity (W/m.deg.)
q <sup>∞</sup>	Volumetric heat generation rate (W/m <sup>3</sup> )
NF	Number of fuel layers
NC	Number of cladding layers
r	Radial distance (m)
R <sub>o</sub>	Cladding outer radius (m)
R <sub>F</sub>	Fuel radius (m)
T	Temperature (°K)
z	Vertical distance measured from fuel rod center
Z	Vertical distance measured from the bottom of fuel rod
ρ	Density (Kg/m <sup>3</sup> )
θ	Time (seconds)
ΔR	Thickness of a cylindrical layer (m)

## SUBSCRIPTS

F	Fuel	c	Cladding / center
f	fluid (coolant)		

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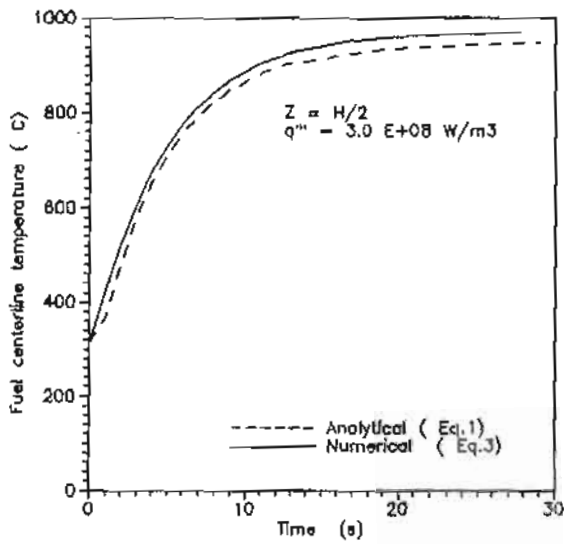


Fig. (2) Comparison between analytical and numerical solutions

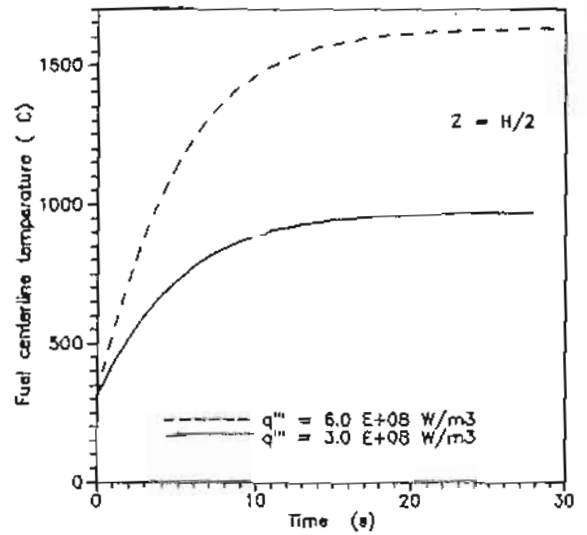


Fig. (3) Fuel temperature behavior for different heat generation rates

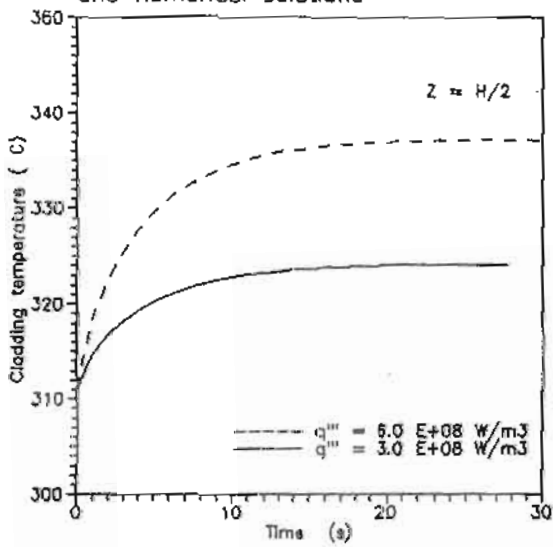


Fig. (4) Cladding temperature behavior for different heat generation rates